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\* WELCOME TO THE \*  
\* U.S. PATENT TEXT FILE \*  
\*\*\*\*\*

=> s dry or dried

295981 DRY  
298445 DRIED  
L1 432819 DRY OR DRIED

=> s granul?

L2 117920 GRANUL?

=> s biomass

L3 3766 BIOMASS

=> s I1(20a) I2 (20a) I3

L4 13 L1(20A) L2 (20A) L3

=> d I4 kwic

US PAT NO: 5,759,562 [IMAGE AVAILABLE] L4: 1 of 13

DETDESC:

DETD(8)

Fungal . . . was provided by mixing the clay mixture and fungal biomass with the nutrient in the ratio of 50:33:17 clay mixture:nutrient:fungal \*\*biomass\*\* by weight before preparing the paste for extrusion. The  $\phi$ granules $\beta$  were air- $\phi$ dried $\beta$  for approximately 18 hours in a fume hood.

=> d kwic 2-13

US PAT NO: 5,431,933 [IMAGE AVAILABLE] L4: 2 of 13

SUMMARY:

BSUM(25)

When very pure fermentations are carried out (with only small residues of organic substances), the broth may even be  $\phi$ dried $\beta$  to an easily handled  $\phi$ granulate $\beta$  without the  $\phi$ biomass $\beta$  and substantially without auxiliary substances such as additional (mineral) carriers. Moreover, fermentation broths which, from the start, are treated in . . .

US PAT NO: 5,418,164 [IMAGE AVAILABLE] L4: 3 of 13

SUMMARY:

BSUM(62)

The cell  $\phi$ granulates $\beta$  are  $\phi$ dried $\beta$  by dehydration of the microorganisms. The customary methods for drying the  $\phi$ biomass $\beta$  by means of heat transfer by convection, such as, for example, current and fluidized bed drying, or by means of . . .

US PAT NO: 5,254,253 [IMAGE AVAILABLE] L4: 4 of 13

DETDESC:

DETD(23)

The . . . a period of time with the specified wastewater feed for a particular installation, until acclimated. Over time, some of the  $\phi$ biomass $\beta$  is saved as cultures in a  $\phi$ granular $\beta$  or  $\phi$ dried $\beta$  material, or in an auxiliary reactor. Saved  $\phi$ biomass $\beta$  can be added to augment the existing  $\phi$ biomass $\beta$  as the occasion demands during periods of shock loading or after a prolonged period of inactivity due to lack of . . .

US PAT NO: 5,068,105 [IMAGE AVAILABLE] L4: 5 of 13

DETDESC:

DETD(53)

A  $\phi$ granular $\beta$  preparation of 50.0 gm commercial fine vermiculite (grade 2) was  $\phi$ dried $\beta$  at 80.degree. -90.degree. C. for 48 hours, and then mixed with 10.0 gm dry weight equivalent of fungal  $\phi$ biomass $\beta$  from the "dried preparation" described above. An equal amount of dried vermiculite was mixed with 10.0 gm dry weight equivalent . . .

US PAT NO: 4,992,179 [IMAGE AVAILABLE] L4: 6 of 13

DETDESC:

DETD(45)

A glass column is employed which contains the  $\phi$ biomass $\beta$   $\phi$ granules $\beta$  at a specified depth. The  $\phi$ dry $\beta$  weight of the  $\phi$ granules $\beta$  is recorded. A solution at a specified metal concentration is pumped in the upflow direction through the column. Using this . . .

DETDESC:

DETD(72)

Increasing the glyoxal content from 0.5% to 5% by weight resulted in the formation of harder  $\phi$ granules $\beta$ . In adding the glyoxal to  $\phi$ dried $\beta$  caustic-treated *B. subtilis*-like  $\phi$ biomass $\beta$ , 125 grams were suspended in 500 ml of glyoxal solution, the amount of glyoxal being sufficient to provide the desired . . .

DETDESC:

DETD(73)

The solution with the  $\phi$ biomass $\beta$  was decanted and the treated  $\phi$ granules $\beta$  were  $\phi$ dried $\beta$  at 80.degree. to 100.degree. C. The residue is either reground, or sieved, or simply crushed to obtain the desired particle. . .

CLAIMS:

CLMS(5)

5. . .  
reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said  $\phi$ biomass $\beta$  reaction product is washed,  $\phi$ dried $\beta$  to a hard grindable body and ground to  $\phi$ granular $\beta$  form and immobilized in an insoluble binder, contacting said solution with an amount of said granular  $\phi$ biomass $\beta$  reaction product sufficient to sorb said cation into said biomass product, and thereafter separating the resulting metal-containing biomass from said solution.

CLAIMS:

CLMS(13)

13. . .  
reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said  $\phi$ biomass $\beta$  product is washed,  $\phi$ dried $\beta$  to a hard grindable body and ground to  $\phi$ granular $\beta$  form and immobilized in an insoluble binder, to provide a variety of particle sizes which are disposed in an upflow. . .

CLAIMS:

CLMS(15)

15. . .  
reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said  $\phi$ biomass $\beta$  reaction product is washed,  $\phi$ dried $\beta$ , and immobilized in an insoluble binder, contacting said solution with an amount of said  $\phi$ biomass $\beta$  reaction product in  $\phi$ granular $\beta$  form sufficient to sorb said cation into said  $\phi$ biomass $\beta$  product, and thereafter separating the resulting metal-containing  $\phi$ biomass $\beta$  from said solution.

CLAIMS:

CLMS(19)

19. . .  
reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said  $\phi$ biomass $\beta$  reaction product is washed,  $\phi$ dried $\beta$ , and immobilized in an insoluble binder, contacting said solution with an amount of said  $\phi$ biomass $\beta$  reaction product in  $\phi$ granular $\beta$  form sufficient to sorb said cation into said  $\phi$ biomass $\beta$  product, and thereafter separating the resulting metal-containing  $\phi$ biomass $\beta$  from said solution.

CLAIMS:

CLMS(26)

26. . .  
reaction product consisting essentially of material derived from the

cell walls thereof having enhanced metal uptake properties following which said *obiomass* reaction product is washed, *odried*, and immobilized in an insoluble binder to provide a hard grindable body and ground to *ogranular* form to provide a variety of particle sizes which are disposed in an upflow column, and passing said solution through said. . .

CLAIMS:

CLMS(27)

27. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said *obiomass* reaction product is washed, *odried* and immobilized in an insoluble binder, contacting said solution with an amount of said *obiomass* reaction product in *ogranular* form sufficient to sorb said cation into said *obiomass* product, and thereafter separating the resulting metal-containing *obiomass* from said solution.

CLAIMS:

CLMS(31)

31. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said *obiomass* reaction product is washed, *odried* and immobilized in an insoluble binder to provide a hard grindable body and ground to *ogranular* form to provide a variety of particle sizes which are disposed in an upflow column, and passing said solution through said. . .

CLAIMS:

CLMS(33)

33. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said *obiomass* reaction product is washed, *odried* and immobilized in an insoluble binder, contacting said solution with an amount of said *obiomass* reaction product in *ogranular* form sufficient to sorb said cation into said *obiomass* product, and thereafter separating the resulting metal-containing *obiomass* from said solution.

US PAT NO: 4,898,827 [IMAGE AVAILABLE] L4: 7 of 13

DETDESC:

DET(42)

A glass column is employed which contains the *obiomass* *ogranules* at a specified depth. The *odry* weight of the *ogranules* is recorded. A solution at a specified metal concentration is pumped in the upflow direction through the column. Using this. . .

DETDESC:

DET(69)

Increasing the glyoxal content from 0.5% to 5% by weight resulted in the formation of harder *ogranules*. In adding the glyoxal to *odried* caustic-treated *B. subtilis*-like *obiomass*, 125 grams were suspended in 500 ml of glyoxal solution, the amount of glyoxal being sufficient to provide the desired. . .

DETDESC:

DET(70)

The solution with the *obiomass* was decanted and the treated *ogranules* were *odried* at 80.degree. to 100.degree. C. The residue is either reground, or sieved, or simply crushed to obtain the desired particle. . .

US PAT NO: 4,824,829 [IMAGE AVAILABLE] L4: 8 of 13

SUMMARY:

BSUM(11)

The . . . in a fine stream or spray onto the carrier while blending. The mixture is blended until homogeneous, resulting in a *odry* *ogranular* non-dusting premix. Alternatively, the premix compositions of the invention may be prepared from crude *obiomass* material by extraction of the biomass into said physiologically acceptable alcohol and utilizing the alcohol extract directly in the preparation. . .

US PAT NO: 4,789,481 [IMAGE AVAILABLE]

L4: 9 of 13

DETDESC:

DET(23)

A glass column is employed which contains the *obiomass* *ogranules* at a specified depth. The *odry* weight of the *ogranules* is recorded. A solution at a specified metal concentration is pumped in the upflow direction through the column. Using this. . .

CLAIMS:

CLMS(5)

5. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said *obiomass* reaction product is washed, *odried* to a hard grindable body and ground to *ogranular* *obiomass* reaction product sufficient to sorb said cation into said *obiomass* product, and thereafter separating the resulting metal-containing *obiomass* from said solution.

CLAIMS:

CLMS(11)

11. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said *obiomass* product is washed, *odried* to a hard grindable body and ground to *ogranular* form, to provide a variety of particle sizes which are disposed in an upflow column, and passing said solution through said. . .

CLAIMS:

CLMS(20)

20. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said *obiomass* reaction product is washed, *odried* to a hard grindable body and ground to *ogranular* form to provide a variety of particle sizes which are disposed in an upflow column, and passing said solution through said. . .

CLAIMS:

CLMS(24)

24. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said *obiomass* reaction product is washed, *odried* to a hard grindable body and ground to *ogranular* form to provide a variety of particle sizes which are disposed in an upflow column, and passing said solution through said. . .

US PAT NO: 4,752,301 [IMAGE AVAILABLE]

L4: 10 of 13

CLAIMS:

CLMS(4)

4. A method according to claim 3 in which the *obiomass* is *odried* by a sprayer to form a powder or in a fluidised bed to form *ogranules*.

US PAT NO: 4,690,894 [IMAGE AVAILABLE]

L4: 11 of 13

DETDESC:

DET(23)

A glass column is employed which contains the *obiomass* *ogranules* at a specified depth. The *odry* weight of the *ogranules* is recorded. A solution at a specified metal concentration is pumped in the upflow direction through the column. Using this. . .

US PAT NO: 4,539,036 [IMAGE AVAILABLE]

L4: 12 of 13

SUMMARY:

BSUM(15)

The . . . preparation is either known or can be effected analogously to known processes. An example of a commercially available fungal mycelium *obiomass* is the *odried* *ogranular* *obiomass* of the mycelial fungus *Penicillium chrysogenum* (Trade Mark Biosol.RTM.) having the following composition:

CLAIMS:

CLMS(17)

17. A method of claim 1 in which the fungal biomass is the dried granular biomass of the mycelial fungus *Penicillium chrysogenum*.

US PAT NO: 4,447,534 [IMAGE AVAILABLE]

L4: 13 of 13

CLAIMS:

CLMS(3)

3. A method in accordance with claim 1, wherein unfermented biomass, together with remaining unfermented nutrients, are removed from the fluidized bed in the form of wet granules, and the granules are subsequently dried.

=> d 1-

1. 5,759,562, Jun. 2, 1998, Compositions for control of soil pests; David John Rhodes, et al., 424/409, 93.5, 405, 408, 410, 418, 421, 489 [IMAGE AVAILABLE]

2. 5,431,933, Jul. 11, 1995, Animal feed supplement based on a fermentation broth amino acid, a process for its production and its use; Wolfram Binder, et al., 426/60, 2, 656; 435/106 [IMAGE AVAILABLE]

3. 5,418,164, May 23, 1995, Self-supporting carrier-free cell granulates for combating pests and treating plants; Wolfram Andersch, et al., 435/254.1; 424/93.5; 435/261, 911 [IMAGE AVAILABLE]

4. 5,254,253, Oct. 19, 1993, Modular shipboard membrane bioreactor system for combined wastewater streams; Henry Behmann, 210/607, 151, 195.2, 195.3, 205, 220, 625, 626, 629 [IMAGE AVAILABLE]

5. 5,068,105, Nov. 26, 1991, Fungal formulation for biocontrol of soilborne plant pathogens; Jack A. Lewis, et al., 424/93.3, 47/57.6, DIG.9; 424/93.5; 435/254.1, 256.3, 256.7, 932, 933, 945 [IMAGE AVAILABLE]

6. 4,992,179, Feb. 12, 1991, Metal recovery; James A. Brierley, et al., 210/661, 75/722; 210/679, 688 [IMAGE AVAILABLE]

7. 4,898,827, Feb. 6, 1990, Metal recovery; James A. Brierley, et al., 435/244; 210/601; 435/252.5, 254.1, 255.2, 256.1, 256.6, 259, 264, 832, 839, 911, 913, 939, 940 [IMAGE AVAILABLE]

8. 4,824,829, Apr. 25, 1989, Non-dusting antibiotic, anticoccidial premix compositions and a process for their manufacture; Irving Klothen, 514/27, 460 [IMAGE AVAILABLE]

9. 4,789,481, Dec. 6, 1988, Metal recovery; James A. Brierley, et al., 210/661, 688; 423/DIG.17 [IMAGE AVAILABLE]

10. 4,752,301, Jun. 21, 1988, Method to due cotton and other substrates with a micro-organism biomass containing Indigo; Werner Koch, 8/653, 646, 918; 435/118, 121 [IMAGE AVAILABLE]

11. 4,690,894, Sep. 1, 1987, Treatment of microorganisms with alkaline solution to enhance metal uptake properties; James A. Brierley, et al., 435/244; 210/601; 435/252.5, 254.1, 255.2, 256.1, 256.6, 259, 264, 822, 839, 911, 913, 939, 940 [IMAGE AVAILABLE]

12. 4,539,036, Sep. 3, 1985, Method of facilitating vegetation; Stefan Naschberger, 71/11, 5, 27, 903; 405/264 [IMAGE AVAILABLE]

13. 4,447,534, May 8, 1984, Method of producing ethanol through fermentation of carbohydrates; Otto Moebus, et al., 435/161, 813, 940 [IMAGE AVAILABLE]

=>

=> s diameter

L5 713838 DIAMETER

=> s I5 and I13

'L13' NOT FOUND

=> s I5 and I4

L6 6 L5 AND L4

=> d I6 kwic 1-

US PAT NO: 5,759,562 [IMAGE AVAILABLE]

L6: 1 of 6

DETDESC:

DETD(4)

A . . . weight until the paste reached a consistency suitable for extrusion. The paste was extruded under pressure through a 0.5 mm diameter Endecott sieve.

DETDESC:

DETD(8)

Fungal . . . was provided by mixing the clay mixture and fungal biomass with the nutrient in the ratio of 50:33:17 clay mixture:nutrient:fungal \*\*biomass\*\* by weight before preparing the paste for extrusion. The granules were air-dried for approximately 16 hours in a fume hood.

US PAT NO: 5,418,164 [IMAGE AVAILABLE]

L6: 2 of 6

SUMMARY:

BSUM(54)

In the process according to the invention, the granulate diameter or granulate stability is controlled by choosing the speed of shaking or rotation of the culture flasks, the number of . . . of 50 rpm to 250 rpm, particularly preferably in a range of 100 to 200 rpm, depending on the granulate diameter or granulate stability. In the case of culture of the microorganisms in fermentation tanks, the stirring speed is preferably kept . . . particular shaking or stirring speed which is most advantageous and leads to the formation of cell granulates with the desired diameter or stability by simple series experiments.

SUMMARY:

BSUM(62)

The cell granulates are dried by dehydration of the microorganisms. The customary methods for drying the biomass by means of heat transfer by convection, such as, for example, current and fluidized bed drying, or by means of . . .

DETDESC:

DETD(15)

The . . . fermentation described above are separated off from the fermentation broth by sieving over a fabric of plastic with a pore diameter of 0.1 mm. An additional content of non-bonded fermentation liquid is separated off by filtration of the cell granulates by . . .

DETDESC:

DETD(40)

granulate of *Metarhizium anisopliae*  
granulate:

according to Example A with a particle size  
of 0.5 to 1.0 mm (diameter)

DETDESC:

DETD(45)

stage

Test cell Cell granulate of *Metarhizium anisopliae*  
granulate: P 0001 with a particle size of 1.0 mm  
(diameter)

DETDESC:

DETD(49)

Cell granulate of *Metarhizium anisopliae*  
granulate: according to Example A with a particle size  
of 0.5 to 1.0 mm (diameter)

DETDESC:

DETD(73)

After . . . the formation of the permanent stages, so-called conidia, starts, these having a length of 9.0 to 12.0 .mu.m and a diameter of 2.0 to 3.0 .mu.m. The conidia are arranged in uniform chains, several strands of chain as a rule lying. . .

DETDESC:

DETD(74)

When . . . also develop yeast-like individual cell stages, so-called

blastospores. The length of the blastospores is 22.0 to 25 .mu.m and their  $\phi$ diameter $\beta$  is 6.0 to 8.0 .mu.m.

CLAIMS:

CLMS(1)

What . . .

class Deuteromycetes, said fungi being capable of mycelium formation, and said granules having an essentially bead shaped structure and a  $\phi$ diameter $\beta$  of about 0.1 to about 1.5 mm.

US PAT NO: 5,254,253 [IMAGE AVAILABLE]

L6: 3 of 6

SUMMARY:

BSUM(33)

The . . . end and cylindrical wall of the element have large pores in the range from 1 mm to 5 mm in  $\phi$ diameter $\beta$ . Compressed air is blown through the open end of the aerator and the energy of the air provides the motive. . .

SUMMARY:

BSUM(44)

It . . . concentrate from the membrane filtration device, to shear incoming gas so as to entrain bubbles of the gas having a  $\phi$ diameter $\beta$ , under pressure, in the range from 1 .mu.m to about 1000 .mu.m (microns), in a stream of microaerated concentrate. The . . .

SUMMARY:

BSUM(50)

(e) . . . the range from about 150 kPa to about 1000 kPa so as to incorporate micronized gas bubbles having an average  $\phi$ diameter $\beta$  in the range from 1 .mu.m to about 1000 .mu.m into said concentrate, forming a microaerated concentrate having separate gas. . .

SUMMARY:

BSUM(65)

It . . . provides all the energy for microaerating the reaction mass with micron-sized bubbles generated through pores less than 20 .mu.m in  $\phi$ diameter $\beta$ , preferably from 0.1 .mu.m to about 1 .mu.m in  $\phi$ diameter $\beta$ , of oxygen-containing gas, at the same time, maintaining necessary recirculation within a liquid bioreaction mass preferably no wider than it . . .

DETDESC:

DET(15)

The . . . about 20 mm, more typically from 50 .mu.m to 10 mm, most of which are greater than 2 mm in  $\phi$ diameter $\beta$ . The micronizer provides a copious supply of oxygen during periods of high oxygen uptake. It is preferred to use both. . .

DETDESC:

DET(23)

The . . . a period of time with the specified wastewater feed for a particular installation, until acclimated. Over time, some of the  $\phi$ biomass $\beta$  is saved as cultures in a  $\phi$ granular $\beta$  or  $\phi$ dried $\beta$  material, or in an auxiliary reactor. Saved  $\phi$ biomass $\beta$  can be added to augment the existing  $\phi$ biomass $\beta$  as the occasion demands during periods of shock loading or after a prolonged period of inactivity due to lack of. . .

DETDESC:

DET(28)

As . . . micrometers), preferably less than 10 .mu.m, through which gas under pressure emerges in a multiplicity of streams each comparable in  $\phi$ diameter $\beta$  to the  $\phi$ diameter $\beta$  of a pore in the metal cylinder.

DETDESC:

DET(35)

Preferred . . . Z8 modules with HSC or TAM membranes. Each such module contains eight (8) 1.83 m long tubes, each having a  $\phi$ diameter $\beta$  of 2.22 cm, connected in series to provide a membrane area of 0.975 m.sup.2/module. The modules themselves are connected. . .

DETDESC:

DET(38)

Concentrate . . . pressure is diffused through micropores into the shearing liquid which generates mainly micron-sized bubbles 49 less than 10 .mu.m in  $\phi$ diameter $\beta$ , in the concentrate, forming a microaerated concentrate stream.

DETDESC:

DET(39)

The . . . to that of the shearing liquid to effect excellent mixing within the diffuser element. In large diffuser elements having a  $\phi$ diameter $\beta$  in excess of about 10 cm, it may be desirable to provide mixing vanes to enhance mixing efficiency and ensure. . .

DETDESC:

DET(45)

An . . . bioreactor, about 1 meter in diam., in which the height of the liquid surface was about 50 cm (height=0.5 times  $\phi$ diameter $\beta$ ).

CLAIMS:

CLMS(1)

I . . .  
the range from about 150 kPa to about 1000 kPa so as to incorporate micronized gas bubbles having an average  $\phi$ diameter $\beta$  in the range from about 1 .mu.m to about 1000 .mu.m into said concentrate, forming a microaerated concentrate having separate . . . bioreaction zone;  
(h) flowing an auxiliary stream of air in the form of coarse bubbles greater than about 2 mm in  $\phi$ diameter $\beta$ , with enough energy to maintain a desirable recirculation pattern in said reaction zone; and, at the same time, directing said. . .

CLAIMS:

CLMS(6)

6 . . . 0.9 Kg O<sub>2</sub>.sub.2 /kWh; bubbles in said microaerated concentrate are in the range from 1 .mu.m to 1000 .mu.m in  $\phi$ diameter $\beta$ ; and, said membrane filtration zone contains a membrane having a pore size in the range from about 0.001 .mu.m-0.5 .mu.m. . .

CLAIMS:

CLMS(7)

7 . . . longitudinally axially into said micronizing zone and said gas is introduced radially therein, passing through pores from 1-100 .mu.m in  $\phi$ diameter $\beta$  in said diffuser element and into said concentrate.

CLAIMS:

CLMS(8)

8 . . . travels longitudinally axially therein, said gas is introduced longitudinally axially therein, passing radially outwardly through pores from 1-100 .mu.m in  $\phi$ diameter $\beta$  in said diffuser element and into said concentrate.

CLAIMS:

CLMS(9)

9 . . .  
with said filtration means;  
(e) auxiliary aeration means providing motive force with relatively coarse bubbles greater than about 2 mm in  $\phi$ diameter $\beta$  introduced below the surface of said bioreactor to establish a recirculation pattern; said gas micronizing means comprising, (i) a tubular microporous. . .

CLAIMS:

CLMS(13)

13 . . . as to microaerate said concentrate infusing it with a multiplicity of gas bubbles in the range from 1-1000 .mu.m in  $\phi$ diameter $\beta$ , and adding the energy of said gas to the kinetic energy of said solids-containing stream so as to provide a. . .  
stream; and,  
(b) flowing an auxiliary stream of air in the form of coarse bubbles greater than about 2 mm in  $\phi$ diameter $\beta$  with enough energy to maintain a desirable recirculation pattern in said reaction zone; whereby activated sludge solids are separated only. . .

CLAIMS:

CLMS(19)

19 . . . longitudinally axially into said micronizing zone and said gas is introduced radially therein, passing through pores from 1-100

.mu.m in diameter in said diffuser element and into said concentrate.

CLAIMS:

CLMS(20)

20. . . . travels longitudinally axially therein, said gas is introduced longitudinally axially therein, passing radially outwardly through pores from 1-100 .mu.m in diameter in said diffuser element and into said concentrate.

US PAT NO: 5,068,105 [IMAGE AVAILABLE] L6: 4 of 6

DETDESC:

DETD(27)

The . . . the form of randomly shaped particles. The particles in grade 2 vermiculite typically are less than about 800.0 microns in diameter, but size will depend on the grade of vermiculite used. The dry preparation has a density of about 0.2 gm/cc.sup.3. . . .

DETDESC:

DETD(53)

A granular preparation of 50.0 gm commercial fine vermiculite (grade 2) was dried at 80.degree.-90.degree. C. for 48 hours, and then mixed with 10.0 gm dry weight equivalent of fungal biomass from the "dried preparation" described above. An equal amount of dried vermiculite was mixed with 10.0 gm dry weight equivalent. . . .

US PAT NO: 4,992,179 [IMAGE AVAILABLE] L6: 5 of 6

DETDESC:

DETD(45)

A glass column is employed which contains the biomass granules at a specified depth. The dry weight of the granules is recorded. A solution at a specified metal concentration is pumped in the upflow direction through the column. Using this. . . .

DETDESC:

DETD(58)

With . . . conducted using a cylindrical column having confined therein a granule bed of the caustic-treated biomass measuring about 1.7 centimeters in diameter and 10 centimeters high, the biomass having a granule size of about -35 mesh +60 mesh. The cadmium solution contained. . . .

DETDESC:

DETD(72)

Increasing the glyoxal content from 0.5% to 5% by weight resulted in the formation of harder granules. In adding the glyoxal to dried caustic-treated *B. subtilis*-like biomass, 125 grams were suspended in 500 ml of glyoxal solution, the amount of glyoxal being sufficient to provide the desired. . . .

DETDESC:

DETD(73)

The solution with the biomass was decanted and the treated granules were dried at 80.degree. to 100.degree. C. The residue is either reground, or sieved, or simply crushed to obtain the desired particle. . . .

CLAIMS:

CLMS(5)

5. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said biomass reaction product is washed, dried to a hard grindable body and ground to granular form and immobilized in an insoluble binder, contacting said solution with an amount of said granular biomass reaction product sufficient to sorb said cation into said biomass product, and thereafter separating the resulting metal-containing biomass from said solution.

CLAIMS:

CLMS(13)

13. . . .

reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said biomass product is washed, dried to a hard grindable body and ground to granular form and immobilized in an insoluble binder, to provide a variety of particle sizes which are disposed in an upflow. . . .

CLAIMS:

CLMS(15)

15. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said biomass reaction product is washed, dried, and immobilized in an insoluble binder, contacting said solution with an amount of said biomass reaction product in granular form sufficient to sorb said cation into said biomass product, and thereafter separating the resulting metal-containing biomass from said solution.

CLAIMS:

CLMS(19)

19. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said biomass reaction product is washed, dried, and immobilized in an insoluble binder, contacting said solution with an amount of said biomass reaction product in granular form sufficient to sorb said cation into said biomass product, and thereafter separating the resulting metal-containing biomass from said solution.

CLAIMS:

CLMS(26)

26. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said biomass reaction product is washed, dried, and immobilized in an insoluble binder to provide a hard grindable body and ground to granular form to provide a variety of particle sizes which are disposed in an upflow column, and passing said solution through said. . . .

CLAIMS:

CLMS(27)

27. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said biomass reaction product is washed, dried and immobilized in an insoluble binder, contacting said solution with an amount of said biomass reaction product in granular form sufficient to sorb said cation into said biomass product, and thereafter separating the resulting metal-containing biomass from said solution.

CLAIMS:

CLMS(31)

31. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said biomass reaction product is washed, dried and immobilized in an insoluble binder to provide a hard grindable body and ground to granular form to provide a variety of particle sizes which are disposed in an upflow column, and passing said solution through said. . . .

CLAIMS:

CLMS(33)

33. . . . reaction product consisting essentially of material derived from the cell walls thereof having enhanced metal uptake properties following which said biomass reaction product is washed, dried and immobilized in an insoluble binder, contacting said solution with an amount of said biomass reaction product in granular form sufficient to sorb said cation into said biomass product, and thereafter separating the resulting metal-containing biomass from said solution.

DETDESC:

DETD(42)

A glass column is employed which contains the biomass granules at a specified depth. The dry weight of the granules is recorded. A solution at a specified metal concentration is pumped in the upflow direction through the column. Using this. . .

DETDESC:

DETD(55)

With . . . conducted using a cylindrical column having confined therein a granule bed of the caustic-treated biomass measuring about 1.7 centimeters in diameter and 10 centimeters high, the biomass having a granule size of about -35 mesh +60 mesh. The cadmium solution contained.

DETDESC:

DETD(69)

Increasing the glyoxal content from 0.5% to 5% by weight resulted in the formation of harder granules. In adding the glyoxal to dried caustic-treated *B. subtilis*-like biomass, 125 grams were suspended in 500 ml of glyoxal solution, the amount of glyoxal being sufficient to provide the desired. . .

DETDESC:

DETD(70)

The solution with the biomass was decanted and the treated granules were dried at 80 degree. to 100 degree. C. The residue is either reground, or sieved, or simply crushed to obtain the desired particle. . .

&gt;&gt; file jpoabs

FILE 'JPOABS' ENTERED AT 13:57:02 ON 04 JUN 1998

\* \* \* \* \* JAPANESE PATENT ABSTRACTS \* \* \* \* \*

\* CURRENTLY, DATA IS LOADED THROUGH DECEMBER 1996, FOR THE \*  
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 \* \* \* \* \*

IRD CNOABS

&gt;&gt; s ;4

ENTER LOGIC EXPRESSION, QUERY NAME, OR (END):end

SEARCH ENDED BY USER

'4' IS NOT A RECOGNIZED COMMAND

&gt;&gt; s i4

38330 DRY  
 55239 DRIED  
 26448 GRANUL?  
 134 BIOMASS  
 L7 1 L1(20A) L2 (20A) L3

&gt;&gt; d i7 all

59-102989 Jun. 14, 1984 L7: 1 of 1  
MANUFACTURE OF FUEL PELLET

INVENTOR: MICHIAKI YAMAMOTO  
 ASSIGNEE: NIPPON SEIKOSHOKU KK  
 APPL NO: 57-211345  
 DATE FILED: Dec. 3, 1982  
 PATENT ABSTRACTS OF JAPAN  
 ABS GRP NO: C245  
 ABS VOL NO: Vol. 8, No. 218  
 ABS PUB DATE: Oct. 4, 1984  
 INT-CL: C10L 5/44

ABSTRACT:

PURPOSE: To stabilize the quality, reduce the power consumption and

shorten the time required for reaching the stationary state, by pulverizing a biomass raw material, drying the pulverized biomass raw material, and compression molding the resultant dried biomass raw material under a specific pressure in a specific granulator to form pellets.

CONSTITUTION: A "biomass" raw material, e.g. wood waste, is pulverized and dried or mixed with a synthetic resin, and the resultant dried powder or mixture is compression molded in a granulator 8. In the process, the granulator 8 is kept in a gastight state by means of rotary valves 4, 22, etc. provided in the raw material feeding part on the upstream side of the granulator 8 and a pellet discharging part 20, and steam or high-temperature air is then blown into a part 6, e.g. a mixer, between the rotary valves 4, 22 etc. and the granulator 8 to granulate the biomass raw material powder or mixture in a state of 0.5.approx.10kg/cm.sup.2 (gauge pressure) saturated steam pressure therebetween in the form of pellets.

&gt;&gt; file epoabs

FILE 'EPOABS' ENTERED AT 13:57:43 ON 04 JUN 1998

\* \* \* \* \* EUROPEAN PATENT ABSTRACTS \* \* \* \* \*

&gt;&gt; s i4

21935 DRY  
 12252 DRIED  
 14035 GRANUL?  
 1010 BIOMASS  
 L8 0 L1(20A) L2 (20A) L3

&gt;&gt; file jpoabs

FILE 'JPOABS' ENTERED AT 13:58:09 ON 04 JUN 1998

\* \* \* \* \* JAPANESE PATENT ABSTRACTS \* \* \* \* \*  
 \* CURRENTLY, DATA IS LOADED THROUGH DECEMBER 1996, FOR THE \*  
 \* JAPANESE PATENT OFFICE ABSTRACTS (JPOABS) AND THROUGH \*  
 \* JANUARY 27, 1998, FOR THE GLOBAL PATENT INFORMATION \*  
 \* JAPANESE PATENT OFFICE (GPI-JPO) FILE. THANKS. \*  
 \* \* \* \* \*

IRD CNOABS

&gt;&gt; d his

(FILE 'USPAT ENTERED AT 13:35:57 ON 04 JUN 1998)

L1 432819 S DRY OR DRIED  
 L2 117920 S GRANUL?  
 L3 3766 S BIOMASS  
 L4 13 S L1(20A) L2 (20A) L3  
 L5 713838 S DIAMETER  
 L6 6 S L5 AND L4

FILE 'JPOABS' ENTERED AT 13:57:02 ON 04 JUN 1998

L7 1 S L4

FILE 'EPOABS' ENTERED AT 13:57:43 ON 04 JUN 1998  
 L8 0 S L4

FILE 'JPOABS' ENTERED AT 13:58:09 ON 04 JUN 1998

&gt;&gt; s i1 and i2

38330 DRY  
 55239 DRIED  
 26448 GRANUL?  
 L9 3563 L1 AND L2

&gt;&gt; s fungus or fungi or fungal

1402 FUNGUS  
 1783 FUNGI  
 245 FUNGAL  
 L10 3154 FUNGUS OR FUNGI OR FUNGAL

&gt;&gt; s i9 and i10

L11 9 L9 AND L10

&gt;&gt; d i11 all 1-

08-302368 Nov. 19, 1996 L11: 1 of 9  
METHOD FOR CONVERTING GENERAL GARBAGE INTO SOLID FUEL

INVENTOR: YOJI OGAKI, et al. (5)  
ASSIGNEE: NKK CORP, et al. (1)  
APPL NO: 07-129618  
DATE FILED: Apr. 28, 1995  
PATENT ABSTRACTS OF JAPAN  
ABS GRP NO:  
ABS VOL NO:  
ABS PUB DATE:  
INT-CL: C10L 5/46; B09B 3/00

#### ABSTRACT:

PURPOSE: To decrease the load on a crusher, prevent the rotting, bad odor, and proliferation of microorganisms and fungi during storage of a solid fuel produced, and eliminate hydrogen chloride gas during combustion in a process for converting general household garbage into a solid fuel.

CONSTITUTION: A raw material 1, i.e., general household garbage, is stored in a pit and crane 2 at the storing step, subjected to the primary crushing 3 to a  $\phi$ granular $\beta$  size of e.g. 75-100mm, subjected to magnetic sorting 4 and aluminum sorting 12 to remove iron and aluminum, subjected to sieving 5 with a 20-30mm-mesh sieve to be separated into oversize garbage and undersize residue. The oversize garbage is subjected to the secondary crushing 6 to a  $\phi$ granular $\beta$  size of 20-30mm, and the undersize residue is mixed 7 with 5-10wt % (based on the  $\phi$ dry $\beta$  residue) lime 8. Then, the oversize garbage after the secondary crushing and the undersize residue contg. lime are subjected to drying and mixing 9, subjected to vol. reduction and solidification 10, and molded into a solid fuel 11.

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07-89807 Apr. 4, 1995 L11: 2 of 9  
METHOD FOR PRODUCING ANTIMICROBIAL SHEET AND METHOD FOR  
PRODUCING  
ANTIMICROBIAL SINTERED COMPACT

INVENTOR: TATSUYA SAEKI  
ASSIGNEE: SEKISUI PLASTICS CO LTD  
APPL NO: 05-238444  
DATE FILED: Sep. 24, 1993  
PATENT ABSTRACTS OF JAPAN  
ABS GRP NO:  
ABS VOL NO:  
ABS PUB DATE:  
INT-CL: A01N 25/34; A01N 25/08; A01N 59/16

#### ABSTRACT:

PURPOSE: To produce an antimicrobial sheet showing good flexibility and capable of exhibiting excellent antimicrobial characteristics by combining amorphous calcium phosphate particles with the ions of an antimicrobial metal,  $\phi$ granulating $\beta$  the mixture, and subsequently shaping the  $\phi$ granules $\beta$  into the sheet, and furthermore to produce an antimicrobial sintered compact high in reliability by using the sheet.

CONSTITUTION: A calcium hydroxide suspension is mixed with a water-soluble high-molecular dispersant and subsequently adjusted to a pH of 10-5 by the dropwise addition of an aqueous phosphoric acid solution to produce a slurry containing amorphous calcium phosphate particles. The slurry is mixed with the ions of an antimicrobial metal and subsequently  $\phi$ granulated $\beta$  into the antimicrobial  $\phi$ granules $\beta$ . The  $\phi$ granules $\beta$  are kneaded with a solvent and a binder and then molded into a sheet-like article. The sheet-like article is  $\phi$ dried $\beta$  to provide the antimicrobial sheet from which the solvent has been removed. The sheet is sintered in an oxidative atmosphere to afford the antimicrobial sintered compact comprising the sintered antimicrobial  $\phi$ granules $\beta$ . The sheet is sintered at 800-1100 $^{\circ}$ C in an oxidative atmosphere to obtain the antimicrobial sintered compact in which the antimicrobial  $\phi$ granules $\beta$  have been sintered in a porous state. The antimicrobial sheet and the antimicrobial sintered compact can be used for retaining the freshness of fresh foods, etc., or for preventing bacteria and fungi $\beta$  on the back surfaces of the ceiling plates of houses or on the back surfaces of chests of drawers, etc.

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06-55092 Mar. 1, 1994 L11: 3 of 9  
PRODUCTION OF POWDER AND  $\phi$ GRANULAR $\beta$  MATERIAL

INVENTOR: HAJIME SHIMIZU  
ASSIGNEE: HAJIME SHIMIZU, et al. (80)  
APPL NO: 04-207973  
DATE FILED: Aug. 4, 1992  
PATENT ABSTRACTS OF JAPAN  
ABS GRP NO: C1207  
ABS VOL NO: Vol. 18, No. 288  
ABS PUB DATE: Jun. 2, 1994  
INT-CL: B02C 19/06

#### ABSTRACT:

PURPOSE: To enable the long-term preservation of produced powdery and  $\phi$ granular $\beta$  materials without degrading the quality of the powdery and  $\phi$ granular $\beta$  materials and without generating fungi $\beta$  and oxidation of the powdery and  $\phi$ granular $\beta$  materials by charging raw materials into a housing from the upper part thereof and pulverizing the raw materials to prescribed grain sizes while forcibly feeding dehumidified  $\phi$ dry $\beta$  air into the housing from the upper side thereof.

CONSTITUTION: The raw materials (e.g. rocks, agricultural products are charged into the housing 2 having an inverted circular cone shape and while the dehumidified  $\phi$ dry $\beta$  air is forcibly fed into the housing via a supply pipe 5 by a blower, the raw materials are pulverized to the grain sizes down to about 100. $\mu$ m within the housing 2. The inside wall of the housing 2 is formed to a polygon shape of 32 angles and the raw materials fluidized in the housing 2 are processed to a powder and  $\phi$ granular $\beta$  state by the repulsion effect thereof by compressed air. Consequently, the intrusion of the worn dust of crushing blades into the processed powdery and  $\phi$ granular $\beta$  materials and the adverse influence of the friction heat generated during crushing on the powder and  $\phi$ granular $\beta$  materials are obviated.

04-29902 Jan. 31, 1992 L11: 4 of 9  
ANTIFUNGAL AGENT AND  $\phi$ FUNGAL $\beta$  CONTROL USING THE SAME

INVENTOR: NORIO WADA, et al. (1)  
ASSIGNEE: SHINTO PAINT CO LTD, et al. (40)  
APPL NO: 02-137692  
DATE FILED: May 28, 1990  
PATENT ABSTRACTS OF JAPAN  
ABS GRP NO: C0938  
ABS VOL NO: Vol. 16, No. 194  
ABS PUB DATE: May 11, 1992  
INT-CL: A01N 25/12; A01N 25/00; A01N 25/02; A01N 25/10; C08K 7/00; C09D 5/14; D01F 1/10; D06M 23/00

#### ABSTRACT:

PURPOSE: To perform  $\phi$ fungal $\beta$  controlling treatment assuredly effective over a long period of time by incorporating a synthetic fiber or plastic with an antifungal agent smaller in  $\phi$ granular $\beta$  size than conventional agents, or by applying or adding a solvent-dispersed antifungal agent to a material to be treated.

CONSTITUTION: An antifungal agent, open bracket e.g. 2-4-thiazolyl)-benzimidazole, close bracket, is ground to .1 toreq.3. $\mu$ m in size through  $\phi$ dry $\beta$  grinding process using e.g. an airflow pulverizer or wet grinding process, e.g. using a medium, and the resulting  $\phi$ granules $\beta$  (or powder) is directly incorporated in a synthetic fiber or plastic; alternatively, the  $\phi$ granules $\beta$  (powder) is dispersed in a solvent (e.g. ethylene glycol, liquid paraffin) and added or applied to an object, thus performing the objective antifungal treatment. Pulverization of the antifungal agent will prevent the drop-off of its effectiveness in adding to plastics etc., and enable its addition to fine synthetic fibers, thereby the present antifungal method can preferably be applied to water-related utensils for e.g. bathrooms or antifungal clothing covers, etc.

01-101880 Apr. 19, 1989 L11: 5 of 9  
ROCKWOOL CULTIVATION OF 'MATSUTAKE' MUSHROOM

INVENTOR: SEIICHI MURATA  
ASSIGNEE: SEIICHI MURATA  
APPL NO: 62-259170  
DATE FILED: Oct. 14, 1987  
PATENT ABSTRACTS OF JAPAN  
ABS GRP NO: C619  
ABS VOL NO: Vol. 13, No. 315  
ABS PUB DATE: Jul. 18, 1989  
INT-CL: C12N 1/14; A01G 1/04; //C12 N1/14; C12R 1:645

#### ABSTRACT:

PURPOSE: To enable the production of MATSUTAKE mushroom mycelia, by effecting shaking culture of a diluted culture solution containing spores of MATSUTAKE using rockwool as a medium, and continuing the culture of the mycelia formed using concentrated culture solution.

CONSTITUTION: Spores of MATSUTAKE  $\phi$ fungus $\beta$  are subjected to shaking culture in a mixture of dilute culture solution containing saccharides, minerals, hormones and so on, and  $\phi$ granular $\beta$  rockwool at 23.approx.24.degree.C. Then, the resultant liqui mycelia are inoculated to rockwool impregnated with concentrated culture solution, and the cultivation is continued in moisture content of 25.approx.30% at 21.approx.22.degree.C to form mycelia layers. Artificial cultivation of MATSUTAKE mushroom mycelia has been succeeded for the first time, by the inventors, using a rockwool utilizing its properties. The most effective culture solution has a composition of 1,000cc of water, 5.approx.10g of honey, 20g of glucose, 5g of  $\phi$ dried $\beta$  yeast, 1g of ammonium tartrate,

1g of potassium phosphate, 0.2g of potassium chloride, 1mg of zinc sulfate, 0.5mg of nicotine, 0.5mg of folic acid, 0.1mg of thiamine hydrochloride, and 0.01mg of indoleacetic acid, and a pH of 4.

61-287527 Nov. 27, 1986 L11: 6 of 9  
HYPERTENSION-SUPPRESSING AGENT COMPOSED OF FOMES JAPONICUS

INVENTOR: AKIMI KADOTA  
ASSIGNEE: OSAKA CHEM LAB  
APPL NO: 60-108550  
DATE FILED: May 20, 1985  
PATENT ABSTRACTS OF JAPAN  
ABS GRP NO: C417  
ABS VOL NO: Vol. 11, No. 132  
ABS PUB DATE: Apr. 24, 1987  
INT-CL: A61K 35/84

#### ABSTRACT:

PURPOSE: To provide an agent for suppressing hypertension by using *Fomes japonicus* as essential component.

CONSTITUTION: *Fomes japonicus* (a "fungus" belonging to Polyporaceae family, *Gododera lucidum*) is dried, crushed in the form of mince, frozen at 10°C, and crushed with a ball mill in frozen state. The crushed product is returned to normal temperature and sieved to collect the fraction between 10 mesh and 200 mesh. The fraction coarser than 10 mesh is frozen again, and crushed with a ball mill. The fraction having the above size is sterilized at low temperature to obtain an agent for hypertension. As an alternative method, *Fomes japonicus* is extracted with water or acetone. The powder or extract is formed in the form of powder, granule, or tablet, optionally together with additives such as diluent, sweetener, excipient, etc.

60-251841 Dec. 12, 1985 L11: 7 of 9  
LIPOMETABOLIC FOOD

INVENTOR: TOSHIO HORIUCHI, et al. (1)  
ASSIGNEE: KK HORIUCHI, et al. (1)  
APPL NO: 59-109166  
DATE FILED: May 29, 1984  
PATENT ABSTRACTS OF JAPAN  
ABS GRP NO: C345  
ABS VOL NO: Vol. 10, No. 128  
ABS PUB DATE: May 13, 1986  
INT-CL: A23F 3/06

#### ABSTRACT:

PURPOSE: To obtain a lipometabolic food, by treating semi-fermented or fermented tea leaves with hot water, drying and pulverizing the product, and using the powder as an essential component.

CONSTITUTION: Semi-fermented tea leaves (commercially available oolong tea) or fermented tea leaves (commercially available black tea) are immersed in hot water of about 100 degrees C. for about 10sec to effect the hot-water treatment. The fungi, etc. attached to the tea leaves are killed by the treatment. The treated tea leaves are dried spontaneously or at a low temperature, and pulverized to 40.approx.100mesh. The powder is formed in the form of powder, granule, etc. The lipometabolic function can be improved remarkably by taking 1.approx.3g of the food daily.

60-23391 Feb. 5, 1985 L11: 8 of 9  
EXTRACT OF FLAMMULINA VELUTIPES

INVENTOR: SADAO NAKAGAKI  
ASSIGNEE: YAMAJIRUSHI JIYOUZOU KK  
APPL NO: 58-127854  
DATE FILED: Jul. 15, 1983  
PATENT ABSTRACTS OF JAPAN  
ABS GRP NO: C286  
ABS VOL NO: Vol. 9, No. 138  
ABS PUB DATE: Jun. 13, 1985  
INT-CL: C07G 17/00; A61K 35/84

#### ABSTRACT:

PURPOSE: To obtain the titled extract for oral administration, containing a carcinostatic and immunity promoting component, keeping the taste, flavor, minor active components, etc. of the original fungi, by concentrating aqueous extract of *Flammulina velutipes* (an edible fungi), removing the precipitate, and drying and forming the concentrate in the form of powder or granule.

CONSTITUTION: For example, a mixture for a culture medium composed of the fruit body or mycelia of *Flammulina velutipes* and chaff, sawdust, rice bran, etc. is added with about 3 times weight of water, and heated. The obtained extract liquid is concentrated with e.g. a vacuum hot kneader,

etc., and centrifuged to remove the precipitate and foreign materials. The supernatant liquid is added with dextrin, dried by vacuum freeze-drying, etc., and formed to powder or granule e.g. with a pulverizer.

59-183669 Oct. 18, 1984 L11: 9 of 9  
SHIITAKE TABLETS AND THEIR PRODUCTION

INVENTOR: HARUMUTSU INOMATA  
ASSIGNEE: MITSUYO INOMATA  
APPL NO: 58-57814  
DATE FILED: Apr. 4, 1983  
PATENT ABSTRACTS OF JAPAN  
ABS GRP NO: C267  
ABS VOL NO: Vol. 9, No. 41  
ABS PUB DATE: Feb. 21, 1985  
INT-CL: A23L 1/212; A61K 9/20; A61K 35/78

#### ABSTRACT:

PURPOSE: The titled tablets which are prepared by compression-molding a powder and extract of SHIITAKE mushroom, keeping their water content at a certain level, thus enabling the effective utilization of low-grade or less valuable SHIITAKES and giving a health food that can be readily taken, because it is in the form of tablets.

CONSTITUTION: A SHIITAKE powder is combined with an extract of SHIITAKE resulting from extraction with water or a mixture thereof with extracts of shelf fungi (SARUNKOSHIIKAKE) and/or *Formes japonicus* fungi (REISHI or MANNENTAKE), when necessary, a molding aid is added to the mixture in an amount of 2.approx.8g per kg. of the SHIITAKE powder to form granules by the wet process. Then, the granules are crushed and dried to 10.approx.18wt% water content, then subjected to compression molding to give the objective tablets.

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FILE 'EPOABS' ENTERED AT 14:01:40 ON 04 JUN 1998

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• EUROPEAN PATENT ABSTRACTS •  
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=> s I11

21935 DRY  
12252 DRIED  
14035 GRANUL?  
619 FUNGUS  
1981 FUNGI  
1145 FUNGAL  
L12 7 L9 AND L10

=> d all I12

US 05074902A Dec. 24, 1991 L12: 1 of 7  
• Granular products containing fungi encapsulated in a wheat gluten matrix for biological control of weeds

INVENTOR: JR WILLIAM J CONNICK, et al. (1)  
ASSIGNEE: CONNICK JR WILLIAM J, et al. (1)  
APPL NO: US 56079190A  
DATE FILED: Jul. 30, 1990  
PATENT ABSTRACTS OF EUROPE  
ABS GRP NO:  
ABS VOL NO:  
ABS PUB DATE:  
INT-CL: A01N 25/12; A01N 63/04

#### ABSTRACT:

Weed pathogenic fungi to be encapsulated in a wheat gluten matrix are blended with flour and water to make a cohesive dough. The dough is extruded, rolled out into a sheet, or otherwise shaped, and dried to form products that contain the fungi entrapped throughout the gluten matrix. The encapsulated fungi grow onto the surface of said products when provided with sufficient light and water. The products of this invention may be used to infect and kill weeds.

=> d-2 all

US 04734393A Mar. 29, 1988 L12: 2 of 7  
Non-clay oil and grease absorbent

INVENTOR: H EDWARD LOWE, et al. (2)  
ASSIGNEE: LOWE H EDWARD  
APPL NO: US 74874885A  
DATE FILED: Jun. 20, 1985

PATENT ABSTRACTS OF EUROPE  
ABS GRP NO:  
ABS VOL NO:  
ABS PUB DATE:  
INT-CL:

ABSTRACT:

An oil and grease absorbent material formed from treated paper sludge or other fibrous slurries and a method of treating the slurry to form the material which includes the physical properties of clay absorbents. The method involves the addition of materials to the shredded slurry to control color, bacteria, fungi, and density. A quantity of lipophilic ray cells are added to the slurry to increase oil absorbency. The slurry is then formed into granules and dried before packaging.

US 04721059A Jan. 26, 1988 L12: 3 of 7  
Nonclay catbox filler

INVENTOR: H EDWARD LOWE, et al. (1)  
ASSIGNEE: LOWE H EDWARD  
APPL NO: US 90196386A  
DATE FILED: Aug. 27, 1986  
PATENT ABSTRACTS OF EUROPE  
ABS GRP NO:  
ABS VOL NO:  
ABS PUB DATE:  
INT-CL:

ABSTRACT:

A clay-like filler material formed from treated paper sludge or other fibrous slurries and a method of treating the sludge to form the filler which includes the physical properties of clay fillers. The method involves adding materials to the shredded slurry to control color, bacteria, fungi, absorbency, pests, and fragrance. The slurry is then formed into granules and dried prior to being packaged.

US 04067821A Jan. 10, 1978 L12: 4 of 7  
Method of treating a biomass

INVENTOR: VACLAV VOTAKEK, et al. (3)  
ASSIGNEE: CESKOSLOVENSKA KOMISE ATOM  
APPL NO: US 66890276A  
DATE FILED: Mar. 22, 1976  
PATENT ABSTRACTS OF EUROPE  
ABS GRP NO:  
ABS VOL NO:  
ABS PUB DATE:  
INT-CL: C02B 1/32

ABSTRACT:

<CHG DATE=19940730 STATUS=O> A technique is described for stiffening a biomass comprising mycelia fungi used for retention of heavy metal ions. The procedure involves dispersing a dry or native mycelium strain in a non-polar dispersion medium, agglomerating the resultant dispersion by adding a stiffening component and a surface active agent, and catalyzing the agglomerated mixture to yield stiffened granules.

WO 09525163A1 Sep. 21, 1995 L12: 5 of 7  
METHODS FOR THE PRODUCTION OF FUNGAL SPORES AND COMPOSITIONS THEREOF

INVENTOR: ROBERT DUNCAN CARMICHAEL, et al. (1)  
ASSIGNEE: PHILOM BIOS INC  
APPL NO: CA 09500094W  
DATE FILED: Feb. 24, 1995  
PATENT ABSTRACTS OF EUROPE  
ABS GRP NO:  
ABS VOL NO:  
ABS PUB DATE:  
INT-CL: C12N 3/00; C12N 1/14

ABSTRACT:

Methods are disclosed for a multi-stage two-phase fungal fermentation process for the production of large quantities of fungal spores which can be used as active ingredients in commercial compositions. The first phase of the fermentation process preferentially stimulates the growth of fungal mycelium, and the volume of mycelial biomass produced during this phase can be considerably increased by successive serial transfers of the mycelial biomass to larger vessels. The second phase, i.e., final phase, of the fermentation process preferentially stimulates fungal sporulation and spore production. The fungal spores produced with this invention can be processed into concentrated slurries or dried powders. Commercial compositions that can be prepared with these fungal spore products as active

ingredients, include dry and wettable powders, liquids and granules.

GB 02188651A Oct. 7, 1987 L12: 6 of 7  
Non-clay material granules

INVENTOR: HENRY EDWARD LOWE, et al. (2)  
ASSIGNEE: LOWE HENRY E  
APPL NO: GB 08705107A  
DATE FILED: Mar. 5, 1987  
PATENT ABSTRACTS OF EUROPE  
ABS GRP NO:  
ABS VOL NO:  
ABS PUB DATE:  
INT-CL: D04H 1/00

ABSTRACT:

<CHG DATE=19940730 STATUS=O> A clay-like material is formed from treated paper sludge or other plant fiber slurries. A method of treating the sludge to form a filler which includes the physical properties of clay fillers involves adding materials to the shredded slurry to control colour, bacteria, fungi, absorbency, pests, and fragrance. The slurry is then formed into granules and dried prior to being packaged. The use of the filler for incorporating agricultural chemicals or as a cat litter is described.

DE 04204793C1 Apr. 15, 1993 L12: 7 of 7  
Binding inorganic material for forming heat or sound insulation abrasives etc. - using binder of phenol oxidase and lignin

INVENTOR:  
ASSIGNEE:  
APPL NO: DE 04204793A  
DATE FILED: Feb. 18, 1992  
PATENT ABSTRACTS OF EUROPE  
ABS GRP NO:  
ABS VOL NO:  
ABS PUB DATE:  
INT-CL:

ABSTRACT:

Process for binding inorganic materials, esp. finely divided fibres, spherules, powders, sands and granules, comprises mixing these materials with phenoloxidases and lignin. The bonding agent comprises an aq. soln. of phenoloxidase(s) obt. from bacteria, plant or fungi that degrade lignin, and lignin; such that the dry solids content is 1-50 wt. % (pref. 3-20 wt. %). The inorganic materials are immersed in or sprayed with the aq. binder soln., then dried and pressed at 100-250C (pref. 150-220C). USE - The process is applicable to mineral fibres, ceramics, silica or glass wool, SiC, metal fibres etc., e.g. for the prodn. of thermal or sound insulating panels, abrasives, et

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